Levelised Cost of Hydrogen (LCOH) Calculator Manual

Update of the May 2024 manual

May 2025





Disclaimer

The aim of this manual is to explain the **methodology** behind the **Levelized Cost of Hydrogen (LCOH) calculator**. Moreover, this **manual** also demonstrates how the calculator can be used for estimating the expenses associated with hydrogen production in Europe using **low-temperature electrolysis** considering **different sources of electricity**. This report serves as an update to the previous version published in May 2024.

The default data in the LCOH calculator is based on values provided by Hydrogen Europe and will be continuously updated on an annual basis. This data is based on research conducted by Hydrogen Europe until December 2024 and reflects electricity source data of 2023 and electrolyser CAPEX values for 2024. Accordingly, the manual will also be updated frequently to ensure accuracy and relevance over time. The authors believe that this data comes from reliable sources, but do not guarantee the accuracy or completeness of this information. The information and views set out in this report are those of the author(s) and do not necessarily reflect the official opinion of the Clean Hydrogen JU. Neither the Clean Hydrogen JU, other European Union institutions and bodies, nor any person acting on their behalf may be held responsible for the use which may be made of the information contained therein.

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Version	Date	Description
1.0	May 2024	In this version, data of 2023 and 2022 is used for the electrolysis and electricity default values, respectively.
2.0	May 2025	In this version, data of 2024 and 2023 is used for the electrolysis and electricity default values, respectively. Additionally, an extra user specified value case was added, in which the effect of the cost of capital and the economic lifetime is examined.

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List of abbreviations

Abbreviation	Definition
EHO	European Hydrogen Observatory
LCOH	Levelized Cost of Hydrogen
CAPEX	Capital Expenditures
OPEX	Operational Expenditures
EU27	The 27 countries of the European Union
EFTA	European Free Trade Association (Iceland, Liechtenstein, Norway and Switzerland)
NPV	Net Present Value
SMR	Steam Methane Reforming
CC	Carbon capture
PEM	Proton Exchange Membrane
RES	Renewable Energy Sources
PV	Photovoltaic
RFNBO	Renewable Fuels of Non-Biological Origin

Overview

In the transition towards a sustainable energy future, examining the Levelized Cost of Hydrogen (LCOH) is crucial for the successful integration of renewable hydrogen into the energy mix. The LCOH is a method used to evaluate the total expenses involved in producing hydrogen throughout its entire lifecycle, including both capital (CAPEX) and operational expenditures (OPEX). Considering these costs, LCOH allows to compare different methods of hydrogen production on a common basis. This enables stakeholders, policymakers, and investors to make informed decisions and evaluate the most cost-effective approaches for producing hydrogen.

This report aims to demonstrate the utilization of the LCOH calculator which allows the calculation of hydrogen production costs in Europe by electrolysis with various electricity sources. **The calculator is now set up only for low-temperature water electrolysis,** incl. alkaline and proton exchange membrane (PEM), which are currently the most mature technologies available. The data presented in this report is based on research conducted by Hydrogen Europe until December 2024. The Interactive LCOH calculator can be accessed on the European Hydrogen Observatory website.

The first chapter provides an overview of the LCOH calculator's interface, outlines what the calculator covers and how it functions.

The second chapter offers insights in the calculation methodology that is behind the calculator. In addition, it explains the different default values utilized in the tool and references to the sources.

The final chapter of the manual showcases several use cases to demonstrate the functionality of the LCOH calculator, e.g. when user specified values are utilized as input. Table 1 and Table 2 provide an overview of the use cases examined and their corresponding results.

Use cases overview

Table 1. Use cases overview of comparative cost analyses based on the default values.

Comparative cost analyses with default values					
Use case	Description	Default values affected	LCOH components affected	Result in this situation	
1. Effect of country	Which country allows to produce hydrogen most cost effectively when using wholesale electricity and alkaline electrolysis technology? Germany or Norway?	 Average electricity costs 2. Grid fees 3. Electricity taxes 	1. Electricity costs 2. Grid fees 3. Taxes	Norway has Iower LCOH	
2. Effect of electricity source	Which electricity source is the most cost- effective solution for the production of hydrogen when using alkaline electrolysis in Spain? Wholesale or PV?	 Operating hours Average electricity costs Grid fees Electricity taxes 	All LCOH components	PV has lower LCOH	
3. Combined effect of electricity source and country	Which country and electricity source allows to produce hydrogen most cost effectively when using alkaline electrolysis technology? Malta with PV or Ireland with onshore wind?	 Operating hours Average electricity costs 	All LCOH components	Ireland with onshore wind has lower LCOH	
4. Effect of electrolysis technology	Which electrolysis technology is the most cost-effective when using wholesale electricity in Germany? Alkaline or PEM?	 CAPEX Energy consumption Stack durability Stack degradation 	All LCOH components	Alkaline has lower LCOH	

Table 2. Use case overview of comparative cost analyses based on user specified values.

Comparative cost analyses with user specified values					
Use case	Description	Default values affected	LCOH components affected	Result in this situation	
5. Effect of other electrolysis technology	Based on full year operation in Norway, does solid oxide electrolysis allow to produce hydrogen more cost-effectively compared to alkaline technology?	All values related to electrolysis unit and electricity source apart from installed power, grid fees and taxes	All LCOH components	Alkaline has lower LCOH	
6. Effect of combining multiple electricity sources	Can a combination of PV and wholesale electricity result in a lower LCOH? With alkaline electrolysis in Spain?	 Operating hours Average electricity costs Grid fees Electricity taxes 	All LCOH components	PV + wholesale electricity has a slightly higher LCOH than PV alone	
7. Effect of subsidies and additional revenues	How does the inclusion of subsidies and the sale of oxygen impact the hydrogen production cost? What is the effect on use case 6?	 Electrolyser CAPEX subsidy Hydrogen feed-in tariff or green premium Reduction of grid fees or electricity taxes Oxygen sale price 	1. Subsidies 2. Oxygen	Strong potential impact of subsidies	
New 8. Effect of cost of capital and economic lifetime	What is the impact of a higher cost of capital and lower economic lifetime compared to the default values for alkaline technology in France using wholesale electricity?	1. Cost of capital 2. Economic lifetime	All LCOH components	Default values have lower LCOH	

Introduction

Introduction

This chapter emphasizes the significance of LCOH as a crucial parameter for hydrogen deployment, discusses the key factors

influencing LCOH, and explains the components covered by the calculator and its functionalities.

1.1. LCOH concept

In the constantly changing realm of clean energy, the pursuit of sustainable alternatives to traditional fossil fuels has become increasingly important. Hydrogen, often seen as the fuel of the future, has attracted considerable interest. Nevertheless, to establish hydrogen as a feasible energy or feedstock option, it is essential to understand its financial implications. This is where the LCOH becomes significant. The LCOH is a method used to evaluate the total expenses involved in producing hydrogen throughout its entire lifecycle, including both capital (CAPEX) and operational costs (OPEX).

The LCOH serves as a valuable tool for evaluating hydrogen against alternative energy options and determining its market competitiveness. This metric enables policymakers, investors, and industry players to make well-informed decisions regarding resource allocation and strategies for promoting cost-effective, sustainable hydrogen production.

Several key factors impact the LCOH. Of main importance is the production technology, in

combination with the used energy source. Each production technology, such as steam methane reforming (SMR), potentially combined with carbon capture (SMR+CC), or electrolysis, either with grid connection or with direct connection to a renewable energy source, has its own varying associated costs. Electrolysis with direct connection to renewable energy sources is widely recognized as one of the most sustainable production processes, vet its cost competitiveness strongly varies in function of the electricity price.

For a broader view on the LCOH of the most used production techniques in Europe, including SMR, SMR+CC, grid-connected electrolysis and electrolysis with direct connection to renewable energy sources, please refer to the European Hydrogen Observatory (EHO) report "The European hydrogen market landscape-November 2024", in addition to the corresponding interactive data dashboard on the website. This manual focuses on the functionalities of the LCOH calculator.

1.2. LCOH calculator

The LCOH calculator provided in the EHO is a tool allowing the calculation of hydrogen production costs via low temperature water electrolysis (alkaline or Proton Exchange Membrane (PEM)) in the different EU27 countries, Norway or the UK. A selection of four different electricity sources is provided in the calculator, including grid connection based on wholesale electricity prices, or direct connection to renewable electricity sources such as photovoltaics (PV) and onshore or offshore wind. The calculator allows to either use default values provided by Hydrogen Europe or user specified values. The default values can change depending on the selection of the country and the electricity source. The user specified values do not change automatically and have to be adapted by the user.

Figure 1 provides an overview of the LCOH calculator interface, outlining the input data utilized by the calculator to calculate the various

components contributing to the total LCOH values. The first category of the input data refers to general parameters such as the cost of capital and the economic lifetime. The second category refers to the operational characteristics of the electrolysis unit covering aspects such as the installed power, the investments and the operational costs, the energy consumption and stack durability. The third category encompasses data associated with the electricity source including operating hours of the electrolysis device based on low-cost energy availability, the average electricity costs, grid fees and electricity taxes. Lastly, additional subsidies and revenues can be specified as user specified values.

Using these input data, the LCOH calculator computes the total LCOH in EUR/kg and provides a breakdown by CAPEX, electricity, other OPEX, grid fees, taxes, subsidies, and oxygen revenues, visualized in a waterfall plot.



Figure 1. LCOH calculator interface.

Methodology

Introduction

This chapter provides a comprehensive understanding of the methodology behind the LCOH calculator's functionalities. More specifically, it gives an explanation of the components involved in the calculation of the LCOH, and the data sources utilized by Hydrogen Europe to provide the default values.

2.1. Overview

As introduced in section 1.2., the LCOH is dependent on different cost components such as CAPEX, electricity, other OPEX, grid fees, taxes,

subsidies and oxygen revenues, which are explained in more detail in Table 3.

Table 3. Explanation of the components included in the LCOH calculation.

Component	Explanation		
CAPEX	The CAPEX includes all upfront investments required to establish the hydrogen production facility. This can encompass various components such as equipment and infrastructure costs, land acquisition, etc. CAPEX costs related to the energy source are not included and are part of the electricity costs. Moreover, CAPEX costs related to transport or processing of hydrogen for end-use applications are also not included; only costs related to the production facility are considered.		
Electricity costs	Electricity costs include expenses related to the consumption of electricity during the electrolysis process. They are mainly dependent on the used energy source, in addition to the electrolysis efficiency.		
Other OPEX	Other OPEX reflected in the LCOH include OPEX costs on top of electricity, grid fees and taxes. This includes stack replacements, maintenance, water consumption, etc.		
Grid fees	These are charges imposed by utility companies for the use of their electricity transmission and distribution infrastructure. Grid fees may vary depending on factors such as location, time of use, and the amount of electricity consumed.		

Taxes	Taxes imposed on electricity consumption, including charges related to renewable energy, capacity, environmental impact, nuclear energy and other electricity taxes. Tax rates may vary depending on local regulations and policies.
Subsidies	Financial incentives provided by governments or other entities to promote hydrogen production or support the use of renewable energy sources. Subsidies can include grants, tax credits, or other forms of financial assistance aimed at reducing the cost of hydrogen production.
Oxygen revenues	In electrolysis-based hydrogen production, oxygen and heat are produced as by- products. The calculator allows to include potential revenues from selling oxygen to nearby consumers. This is not the case for excess heat and should be considered separately by the user, if applicable.

2.2. Default values

The LCOH calculator provides the option to make calculations based on default values or user specified values. These default values are provided by Hydrogen Europe, either sourced from literature or from insights of their members. Table 4 presents the various assumptions and sources that were used for deriving the default values that are displayed in the LCOH calculator.

	Table 4.	Assumptions	and sources	for default	values	estimation	in the LCOF	l calculator.
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	Units	Assumptions and sources	
General parameters			
Cost of capital	%	The default cost of capital is set at 6% and the default	
Economic lifetime	Years	economic lifetime at 25 years, based on assumptions of Hydrogen Europe.	
Electrolysis unit			
Installed power	kW	A total size of 20 MWel is considered for deriving the default values of the electrolysis unit. Changing this value	

		does not automatically change other default values, such as CAPEX or OPEX.	
CAPEX Stack replacement costs Other OPEX Energy consumption Stack durability	EUR/kW % CAPEX % CAPEX kWh/kg h	Data are based on research from Hydrogen Europe for electrolyser CAPEX and OPEX values of projects located in EU27, EFTA or UK, based on interviews with developers and other industry sources. Data was sourced from the Clean Hydrogen JU Strategic Research and Innovation Agenda in addition to the Danish	
Stack degradation	% per 1000h	Lifergy Agency reclinology Data for Kenewable ruleis.	
Electricity source Operating hours	h/year	 For wholesale electricity, it is assumed that the 4,000 cheapest operating hours are used. For solar PV, onshore and offshore wind the operating hours are based on capacity factors of the EU Member States from the JRC ENSPRESO model. For directly connected off-grid electrolysis (PV or wind), the electrolyser is scaled down vs. RES power, allowing for a higher electrolysis capacity factor. The following electrolyser capacity factor adjustments are made based on assumptions from Hydrogen Europe: For PV the capacity factor of electrolysis is assumed to be 25% higher than RES For onshore wind the capacity factor of the electrolyser is 11% higher than RES For offshore wind the capacity factor of the electrolyser is the same as RES 	
Average electricity costs	EUR/MWh	• Wholesale electricity costs were sourced from the European network of transmission system operators for electricity (ENTSO-E), by calculating the 4,000 cheapest hours per country (2023 data was used for the LCOH calculator released in January 2025).	

		 Solar PV, onshore and offshore wind electricity costs in Europe are sourced from IRENA's renewable power generation costs (2023 data was used for the LCOH calculator released in January 2025).
Grid fees	EUR/MWh	• The grid fees and electricity taxes are sources from Eurostat based on the 'electricity prices components for non-household consumers' dataset. The price components are extracted for a consumption range of 20,000 MWh - 69,999 MWh. (2023 data was used for the LCOH calculator released in January 2025).
Electricity taxes	EUR/MWh	 By using the Eurostat dataset, the grid fees refer to network costs and the electricity taxes include renewable, capacity, environmental, nuclear and other taxes. For PV and onshore wind, it is assumed that a direct connection to the electrolysis unit is used, excluding grid fees and electricity taxes. For wholesale electricity and offshore wind, it is assumed that grid connection is used, thus including grid fees and electricity taxes.
Subsidies and additional	revenues	
Electrolyser CAPEX Subsidy	EUR/kW	The subsidies and additional revenues are always zero
Hydrogen feed-in tariff or green premium	EUR/kg	under the default values. Any subsidies or additional revenues you might receive for a project, can be captured in
Reduction of grid fees or electricity	EUR/MWh	the user specified values.
Oxygen sale price	EUR/t	

It should be noted that the default data does not show actual hydrogen production costs from operational water electrolysis plants in Europe but is a best estimate of what production costs could be expected given current costs of multiMW state-of-the-art electrolysis system and latest available annual electricity costs.

2.3. Calculations

In order to understand the relationship among the various components comprising the LCOH and their impact on the overall cost of operating the electrolysis unit, several key calculations are involved. The formula for determining the total LCOH (Equation 1) encompasses the consideration of capital expenditures (CAPEX) and various operating expenses (OPEX). These expenses include electricity costs for operating

the electrolysis unit, grid fees, electricity taxes, and other operating expenses as well as revenues from subsidies and oxygen sales.

In order to calculate these different cost components starting from the default values or user specified values, first the hydrogen output and energy consumption of the installation should be known.

$Total \ LCOH \ \left(\frac{EUR}{kg}\right)$

= CAPEX (Eq.7) + Electricity cost (Eq.9) + Other OPEX (Eq.13) + Grid fees (Eq.15) + Taxes (Eq.17) + Subsidies (Eq.22) + Oxygen revenues (Eq.25)

Equation 1. Calculation of the total Levelized Cost of Hydrogen (LCOH) in EUR/kg.

Hydrogen output and energy consumption

As the electrolysis unit operates, the stack it contains degrades over time, thus requiring periodic replacement. The frequency of these replacements depends on factors such as the durability of the stack, the operating hours and the economic lifetime of the installation (Equation 2). In the current version of the calculator (January 2025), the economic lifetime is chosen to be 25 years. Due to degradation of the stack over time, the energy consumption is not constant but progressively increases in time. Therefore, Equation 3 is used to calculate the average energy consumption over the economic lifetime of the project. This energy consumption is also used to derive the total energy consumption of the project (Equation 6). See Appendix A1 for more clarifications on how Equation 3 was derived.

The capacity can be derived from the project size, i.e. electrolysis installed power, and average energy consumption of the installation (Equation 4). The total hydrogen output is then dependent on the operating hours, capacity and economic lifetime of the installation (Equation 5).

Stack replacements (a.u.) = Rounddown

 $\frac{\left(\frac{h}{years} \right) \times Operating \ hours \ \left(\frac{h}{year} \right)}{Stack \ durability \ (h)}$

Equation 2. Calculation of stack replacement during the economic lifetime of the electrolysis unit.

Energy consumption (kWh/kg)
= (Energy Consumption × (1 + (Stack degradation × Stack durability/1000))
+ Energy Consumption)/2 × (Stack replacements × Stack durability)
/(Operating hours × Economic lifetime) + (Energy Consumption × (1
+ (Stack degradation × ((Operating hours × Economic lifetime)
- (Stack replacements × Stack durability))/1000))
+ Energy Consumption)/2 × ((Operating hours × Economic lifetime)
- (Stack replacements × Stack durability))/(Operating hours × Economic lifetime)

Equation 3. Calculation of the average energy consumption per kg hydrogen over the total economic lifetime of the electrolysis unit (kWh/kg).

Capacity
$$\left(\frac{kg}{h}\right) = \frac{Electrolysis installed power (kW)}{Energy consumption per kg \left(\frac{kWh}{kg}\right)}$$

Equation 4. Calculation of the electrolysis unit capacity (kg/h).

Hydrogen output
$$(kg) = 0$$
 perating hours $\left(\frac{h}{year}\right) \times Capacity\left(\frac{kg}{h}\right) \times E$ conomic lifetime (years)

Equation 5. Calculation of electrolysis hydrogen output (kg).

Energy consumption (**MWh**) =
$$\frac{Hydrogen \ output \left(\frac{kg}{h}\right) \times Energy \ consumption \ perkg \left(\frac{kWh}{kg}\right)}{1000}$$

Equation 6. Calculation of the energy consumption (MWh) of the electrolysis unit.

CAPEX

The electrolyser CAPEX is determined by considering the CAPEX in function of the installed power of the electrolysis unit, as outlined in Table 4 and computed using Equation 7.

This electrolyser CAPEX subsequently serves as an input parameter for Equation 9 for the calculation of the CAPEX cost associated with producing each kilogram of hydrogen. It should be noted here that the CAPEX cost component in EUR/kg is also dependent on the cost of capital and the economic lifetime (Equation 8). This considers that money spent today holds greater value compared to the future, as it could potentially be invested elsewhere at a certain rate.

Electrolyser CAPEX (**EUR**) = Electrolysis installed power (kW) × CAPEX

Equation 7. Calculation of the electrolyser CAPEX (EUR) for the establishment of the electrolysis unit.

Cost of capital (a.u.)

 $= Economic \ lifetime \ \times \ \frac{cost \ of \ capital \ (\%) \ \times \ (1 + cost \ of \ capital \ (\%) \)^{economic \ lifetime}}{(1 + cost \ of \ capital \ (\%))^{economic \ lifetime} - 1}$

Equation 8. Calculation of the cost of capital component that increases the CAPEX costs .

$$CAPEX\left(\frac{EUR}{kg}\right) = \frac{Electrolyser\ CAPEX\ (EUR) \times Cost\ of\ capital\ (a.u.)}{Hydrogen\ output\ (kg)}$$

Equation 9. Calculation of the electrolyser CAPEX costs per kilogram of hydrogen produced (EUR/kg).

Electricity

The cost of energy is determined by the energy consumption as defined in Equation 6 and the average electricity costs, which can either be

default values or values specified by the user. No change in electricity costs is considered over the years. This cost of energy is subsequently utilized in Equation 11 to calculate the electricity costs per kilogram of hydrogen produced.

Cost of energy (EUR) = Energy consumption (MWh) × Average electricity costs $\left(\frac{EUR}{MWh}\right)$

Equation 10. Calculation of cost of energy consumed (EUR) by the electrolysis unit.

Electricity cost $\left(\frac{EUR}{kg}\right) = \frac{Cost \ of \ energy \ (EUR)}{Hydrogen \ output \ (kg)}$

Equation 11. Calculation of electricity costs per kilogram of hydrogen produced (EUR/kg).

Other OPEX

Other OPEX reflected in the LCOH cost include both the stack replacement costs and other OPEX, both expressed as a function of CAPEX.

The stack replacement costs are dependent on the number of stack replacements and the cost for a stack replacement, which is expressed by the default or user specified values as a

percentage of the CAPEX costs (Equation 12). Similarly, other OPEX costs are also derived as an annual percentage of the CAPEX costs over the economic lifetime of the project (Equation 13). No changes in the costs for stack replacements or other OPEX are considered over the years. Finally, the output from Equations 12 and 13 is used to calculate the other OPEX costs for each kg of hydrogen produced (Equation 14).

```
Stack replacement costs (EUR)
               = Stack replacement costs (\%CAPEX) \times Electrolyser CAPEX (EUR)
               × Stack replacements (a.u.)
```

Equation 12. Calculation of stack replacement costs (EUR) during the economic lifetime of the electrolysis unit.

Other OPEX (EUR)

= Electrolyser CAPEX (EUR) × Other OPEX $\left(\% \frac{CAPEX}{vear}\right)$ × Economic lifetime (years)

Equation 13. Calculation of other OPEX costs (EUR) for the operation of the electrolysis unit.

 $Other OPEX costs\left(\frac{EUR}{kg}\right) = \frac{(Other OPEX (EUR) + Stack replacements costs (EUR))}{Hydrogen output (kg)}$

Equation 14. Calculation of other OPEX costs per kilogram of hydrogen produced (EUR/kg).

Grid fees

The costs associated with grid fees is dependent on the energy consumption as defined in Equation 6 and the grid fees per MWh, which can either be the default values or values specified by the user. No annual growth rate in grid fees is considered in the calculations. This grid fee cost is then used in Equation 16, along with the hydrogen output, to determine the grid fee costs per kilogram of hydrogen produced

For the default values, as expressed in Table 4, for PV or onshore wind as the electricity source, no grid fees are considered.

Grid fees (**EUR**) = Energy consumption (MWh) × Grid fees $\left(\frac{EUR}{MWh}\right)$

Equation 15. Calculation of grid fees (EUR) for the operation of the electrolysis unit.

Grid fees
$$\left(\frac{EUR}{kg}\right) = \frac{Grid fees (EUR)}{Hydrogen output (kg)}$$

Equation 16. Calculation of grid fees costs per kilogram of hydrogen produced (EUR/kg).

Electricity taxes

As in the case of grid fees, the electricity taxes costs (Equation 17) are influenced by the energy consumption as defined in Equation 6 and the electricity taxes per MWh. Again, no annual grow rate in electricity taxes is considered in the calculations. This electricity taxes cost is then applied in Equation 18, along with the hydrogen output, to determine the electricity taxes costs per kilogram of hydrogen produced.

Also no electricity taxes are considered when using PV or onshore wind as the electricity source, as expressed in Table 4.

Electricity taxes (EUR) = Energy consumption (MWh) × Electricity taxes $\left(\frac{EUR}{MWh}\right)$

Equation 17. Calculation of taxes (EUR) for the operation of the electrolysis unit.

Electricity taxes $\left(\frac{EUR}{kg}\right) = \frac{Electricity taxes (EUR)}{Hydrogen output (kg)}$

Equation 18. Calculation of electricity taxes costs per kilogram of hydrogen produced (EUR/kg).

Subsidies

Hydrogen subsidies can be offered in various ways, either as a grant in function of the installed electrolyser plant (Equation 20), in function of the hydrogen that is produced (Equation 21), or by lowering the electricity costs (e.g. via lower grid fees or electricity taxes, Equation 22). Equation 19 sums up these different kind of subsidies, which is then applied in Equation 23, along with the hydrogen output, to determine the subsidies revenues per kilogram of hydrogen produced. For the CAPEX subsidies, the cost of capital (Equation 8) is taken into account.

Subsidies (**EUR**) = Grants (EUR) + Production subsidies (EUR) + Electricity cost reductions (EUR) Equation 19. Calculation of subsidies revenues (EUR) for the operation of the electrolysis unit.

Grants (EUR) = Electrolyser CAPEX subsidy $\left(\frac{EUR}{kW}\right) \times$ Electrolyser installed power (kW)

Equation 20. Calculation of CAPEX grants in function of the installed electrolyser plant (EUR).

Production subsidies (EUR) = Hydrogen feed in tariff or green premium $\left(\frac{EUR}{kg}\right) \times$ Hydrogen output (kg)

Equation 21. Calculation of the subsidies in function of the hydrogen that is produced (EUR).

Electricity cost reductions (EUR)

= Reduction of electricity $cost\left(\frac{EUR}{MWh}\right) \times Energy \ consumption \ (MWh)$

Equation 22. Calculation of the subsidies related to the reduction of grid fees or electricity taxes (EUR).



Equation 23. Calculation of subsidies revenues per kilogram of hydrogen produced (EUR/kg).

Oxygen revenues

Equation 24 is employed to quantify the oxygen output, a parameter linked to the hydrogen output based on the difference in molar mass. Subsequently, Equation 25 is used to determine the oxygen revenues (in EUR), taking into account both the selling price of oxygen and the quantity produced.

These oxygen revenues are then applied in Equation 26, along with the hydrogen output, to determine the oxygen revenues per kilogram of hydrogen produced. **Oxygen output** (Kg) = Hydrogen output (kg) × 8

 $\left(\frac{EUR}{t}\right)$

Equation 24. Calculation of the oxygen output during the economic lifetime of the electrolysis unit (kg).

Oxygen revenues (EUR) = Oxygen output (kg)
$$\times \frac{Oxygen \text{ sale price}}{10^3}$$

Equation 25. Calculation of the oxygen revenues (EUR) during the economic lifetime of the electrolysis unit.

Oxygen revenues
$$\left(\frac{EUR}{kg}\right) = -1 \times \frac{Oxygen renenues (EUR)}{Hydrogen output (kg)}$$

Equation 26. Calculation of the oxygen revenues per kilogram of hydrogen produced (EUR/kg).

Use cases

Introduction

This chapter presents various use case scenarios to demonstrate how the LCOH calculator can be used illustrating the potential impact of input data on the total LCOH. The goal of the different use cases is to explain all the different functionalities of the calculator, including the selection of the country, electricity source and electrolysis technology for changing the default values, but also the option to make calculations based on user defined values.

3.1.

Overview

The LCOH calculator automatically calculates the different cost components determining the total hydrogen production costs. When calculating using the default values, the output is directly influenced by parameter selections made from the dropdown menu within the calculator, which include:

- Country: 29 options available, namely EU27 countries, Norway and UK.
- Electricity source: 4 options available, namely wholesale, PV, onshore, and offshore wind.

 Electrolysis technology: 2 options available, namely alkaline or PEM.

Users also have the option to input their own values. Note that these user specified values do not update automatically when changing the parameters in the dropdown menu and must thus always be adjusted manually.

Figure 2 illustrates the process for selecting these parameters within the LCOH calculator to determine the total LCOH.

Perform calculations using: • Default values • User specified	Step.1 Select the calculation method: Default or user specified values	 Perform calculations using: Default values User specified User the UK
Select country Germany Select electricity source	•	Select country Germany Austria
Wholesale Select electrolysis technology Alkaline	v l	Belgium Bulgaria Croatia Cyprus Czechia
Perform calculations using: • Default values • User specified	Step.4 Select the electrolysis technology: Alkaline or PEM	 Perform calculations using: Default values User specified Step.3 Select the electricity source: Wholesale, PV, onshore or offshore wind
Select country Germany	•	Select country Germany
Wholesale Select electrolysis technology		Select electricity source Wholesale PV
Alkaline Alkaline PEM		Onshore wind Offshore wind Wholesale

Figure 2. Step-by-step process for selecting parameters within the LCOH calculator.

3.2. Comparative cost analyses with default values

To explore all the different functionalities of the calculator when using default values, four distinct use cases are examined. These cases involve variations on the country, electricity source, and electrolysis technology, as well as a combination of them.

Use case 1 concentrates on the effects of selecting different countries for the same electrolysis technology and electricity source. In use case 2, the evaluation focuses on changing the electricity source with identical electrolysis

technology and country. Use case 3 combines the methodologies of case 1 and case 2, enabling alterations in both the electricity source and the country while holding the electrolysis technology constant. Use case 4 compares the influence of the electrolysis technology selection while keeping the electricity source and country constant.

Table 5 provides an overview of the different use cases examined.

Table 5. Overview of the different use cases based on default data.

Use case	Calculation method	Electrolysis technology	Electricity source	Country
Use case 1 - Effect of country	Default values	Alkaline electrolysis	Wholesale	Germany vs. Norway
Use case 2- Effect of electricity source	Default values	Alkaline electrolysis	Wholesale vs. PV	Spain
Use case 3– Combined effect of country and electricity source	Default values	Alkaline electrolysis	PV vs. onshore wind	Malta vs. Ireland
Use case 4- Effect of electrolysis technology	Default values	Alkaline vs. PEM electrolysis	Wholesale	Germany

Use case 1 - Effect of country

In use case 1, the LCOH in Germany is compared to Norway when using the same electricity source (wholesale) and electrolysis technology (alkaline). This comparison can be useful if the objective is to evaluate the most cost-effective location for producing hydrogen based on a fixed electrolysis technology and electricity source. Selecting Norway when using wholesale electricity also allows the production of RFNBO hydrogen^{1,} since Norway's grid electricity is nearly 100% renewable.

Use case 1: Which country allows to produce hydrogen most cost effectively when using wholesale electricity and alkaline electrolysis technology? Germany or Norway?

As observed in Figure 3, the choice of the country within the LCOH calculator only impacts the

default data related to the electricity source. In this example, the selection of Norway as the country for installing an electrolysis plant demonstrated several advantages over Germany. Norway had 30.37 EUR/MWh lower average electricity costs in 2023, in addition to 21.30 and 24.60 EUR/MWh lower grid fees and electricity taxes, respectively.

As a result, the LCOH calculator output (Figure 4) indicates that for a company intending to establish an electrolysis plant utilizing alkaline technology and operating on wholesale electricity, Norway emerged as the most economically advantageous setting at 5.54 EUR/kg (4.16 EUR/kg cheaper compared to Germany).

In this use case, the country selection had an impact on the electricity, the grid fees and taxes costs components, being 1.65, 1.17 and 1.34 EUR/kg lower for Norway, respectively.

¹ Based on the assumption that the share of renewable electricity in the electricity mix is above 90% in the chosen bidding zone.



The default values changed are related to the electricity source

Average Electricity costs Grid fees Electricity Taxes

Figure 3. Use case 1 - effect of changing the country on the default values.



Figure 4. Use case 1 - effect of changing the country on the LCOH output.

Use case 2 - Effect of electricity source

In use case 2 the electricity sources, wholesale and PV, are compared when using the same electrolysis technology (alkaline) and country (Spain). This comparison can be useful if the objective is to evaluate the most cost-effective electricity source for producing hydrogen in the same country and with identical electrolysis technology.

Spain serves as a compelling case study for examining hydrogen production utilizing PV technology as it is an EU country with abundant solar irradiation. Hydrogen production based on a direct connection between the PV installation and the electrolysis unit, could also be considered as RFNBO hydrogen².

Use case 2: Which electricity source is the most cost-effective solution for the production of hydrogen when using alkaline electrolysis in Spain? Wholesale or PV?

As observed in Figure 5, changing the input in the "Select electricity source" field of the LCOH calculator only impacts the default data related to the electricity source. Utilizing PV technology as the electricity source in Spain offers distinct advantages compared to wholesale electricity. Specifically, PV exhibited 22.45 EUR/MWh lower average electricity costs in 2023, and unlike wholesale, incurs no grid fees or taxes as the calculator considers a direct connection between the PV installation and the electrolysis device. However, the operating hours of the electrolysis device are significantly lower when PV is used as electricity source compared to wholesale.

Despite the lower operating hours, the LCOH calculator output (Figure 6) indicates that the LCOH of the alkaline electrolysis plant utilizing PV technology in Spain is more cost-effective at 5.99 EUR/kg (0.96 EUR/kg lower than wholesale).

Notably, all individual LCOH components are lower with PV as the electricity source, except for CAPEX, which was estimated to be around 1.06 EUR/kg more expensive. This difference in CAPEX can be attributed to the lower operating hours when using PV compared to wholesale. The most significant disparity was observed in electricity costs, with PV being 1.23 EUR/kg lower.

² If the criteria on additionality and temporal and geographic correlation are met.





Figure 5. Use case 2 - effect of changing the electricity source on the default values.



Figure 6. Use case 2 - effect of changing the electricity source on the LCOH output.

Use case 3 – Combined effect of electricity source and country

In use case 3, the LCOH in Malta is compared to Ireland when using PV and onshore wind as the electricity source, respectively. Both projects make use of the same electrolysis technology (alkaline). This comparison can be useful if the objective is to evaluate the most cost-effective combination of location and electricity source for producing hydrogen based on a fixed electrolysis technology.

Use case 3: Which country and electricity source allows to produce hydrogen most cost effectively when using alkaline electrolysis technology? Malta with PV or Ireland with onshore wind?

As observed in Figure 8, changing the country and the electricity source in the LCOH calculator only impacts the default data related to the electricity source. In this example, the selection of Malta as the location for installing an electrolysis plant using photovoltaic power demonstrated a cost advantage of 1.7 EUR/MWh in average electricity costs in 2023 compared to onshore wind in Ireland. However, the installation in Ireland was able to operate for 2,156 more hours annually. In both cases, no grid fees or electricity taxes were imposed.

As a result, the LCOH calculator output (Figure 9) indicates that for a company intending to establish an electrolysis plant utilizing alkaline technology, using onshore wind in Ireland emerged as the most economically advantageous setting at 4.51 EUR/kg (1.73 EUR/kg cheaper compared to PV in Malta).

In this use case, combining the country selection with the electricity source had an impact on the CAPEX, electricity and other OPEX costs components. The most substantial difference lied in CAPEX which was 1.57 EUR/kg lower for onshore wind in Ireland, as a result of the increased operating hours.





Figure 7. Use case 3 - effect of changing the country and the electricity source on the default values.



Figure 9. Use case 3 - effect of changing the country and the electricity source on the LCOH output.

Use case 4 - Effect of electrolysis technology

In Use case 4 alkaline electrolysis is directly compared to PEM electrolysis when using the same electricity source and country. In this example, wholesale electricity is selected as the electricity source and Germany as the country of focus. This comparison can be useful if the objective is to evaluate the most cost-effective electrolysis technology when the country and electricity source have already been selected.

Use case 4: Which electrolysis technology is the most cost-effective when using wholesale electricity in Germany? Alkaline or PEM?

As observed in Figure 10, the choice of electrolysis technology within the LCOH calculator only impacts the default data concerning the characteristics of the electrolysis unit. Specifically, the implementation of alkaline technology demonstrated several advantages over PEM technology. Alkaline technology showcased approximately 193 EUR/kW lower CAPEX costs, 0.9 kWh/kg lower energy

consumption, 0.07%/1000h lower stack degradation rate, and 20,000 h higher stack durability compared to PEM.

As a result, the LCOH calculator output (Figure 11,) indicates that for a company intending to establish an electrolysis plant utilizing wholesale electricity in Germany, alkaline technology emerged as the most cost-effective option at 9.70 EUR/kg (0.53 EUR/kg cheaper compared to PEM).

Notably, all individual cost components contributing to the total LCOH were lower when utilizing alkaline technology. The most substantial difference lied in CAPEX, where it was 0.27 EUR/kg lower, while the variance in the remaining components was less than 0.1 EUR/kg.

Please note that the PEM technology has a faster response time compared to alkaline electrolysis, which should also be taken into account when comparing technologies, in addition to other parameters that are not in scope of this calculator.

	Aikaiiile				PEIVI)	
		Units	Default values			Units	Default va
lculations using: values ecified	General parameters Cost of capital: Economic lifetime:	% Years	6.00% 25	Perform calculations using: • Default values • User specified	General parameters Cost of capital: Economic lifetime:	% Years	6.00% 25
ntry	Electrolysis unit	F/W/	20.000	Select country	Electrolysis unit	F10/	20.000
	CAPEX:	EUR/kW	2,310	Germany	CAPEX:	EUR/kW	2,503
tricity source	Stack durability:	h	80,000	Select electricity source Wholesale	Stack durability:	h	60,000
rolysis technology	Stack degradation: Stack replacement costs:	% per 1000n % CAPEX	15.00%	Select electrolysis technology	Stack degradation: Stack replacement costs:	% per 1000h % CAPEX	0.19%
•	Other OPEX:	% CAPEX	2.00%	PEM	• Other OPEX:	% CAPEX	2.00%
	Electricity source Operating hours:	h/year	4,000		Electricity source Operating hours:	h/vear	4.000
	Average electricity costs:	EUR/MWh	57.78 26.70		Average electricity costs:	EUR/MWh	57.78
	Electricity taxes:	EUR/MWh	33.00		Electricity taxes:	EUR/MWh	33.00
	Subsidies and additional revenues				Subsidies and additional revenues		
	Electrolyser CAPEX subsidy: Hydrogen feed-in tariff or green premium:	EUR/kW EUR/kg	0		Electrolyser CAPEX subsidy:	EUR/kW	0
	Reduction of grid fees or electricity taxes:	EUR/MWh	0		Reduction of grid fees or electricity taxes:	EUR/MWh	0
	Oxygen sale price:	EORA	0		Oxygen sale price:	EUR/t	0

Figure 10: Use case 4 - effect of changing the electrolysis technology on the default values.



Figure 11. Use case 4 - effect of changing the electrolysis technology on the LCOH output.

3.3. Comparative cost analyses of user specified values

Users can utilize this function to extend the capabilities of the LCOH calculator by manually adjusting input data with their own values to calculate the cost of producing hydrogen in Europe. To explore the capability of user specified values, four distinct use cases are examined.

These cases use different parameters for the general parameters, the electrolysis unit and the

electricity source. In use case 5, a case study is made for the use of solid oxide electrolysis, and in use case 6, PV is combined with wholesale electricity to increase the operating hours. Finally in use case 7, the use of subsidies and additional revenues is showcased, while in use case 8, the effect of cost of capital and the economic lifetime is examined. The details of each use case are summarized in Table 6.

Use case	Calculation method	Production method	Electricity source	Country
Use case 5- Effect of other electrolysis technology	User specified values	Solid oxide vs. alkaline electrolysis	Wholesale	Norway
Use case 6– Effect of combining multiple electricity sources	User specified values	Alkaline electrolysis	Combination of PV + wholesale	Spain
Use case 7- Effect of subsidies and additional revenues	User specified values	Alkaline electrolysis + subsidies and additional revenues	Combination of PV + wholesale	Spain
NewUse case 8- Effect of cost of capital and economic lifetime	User specified values	Alkaline electrolysis with different economic lifetime and cost of capital	Wholesale	France

Table 6. Overview of the different use cases.

Use case 5 - Effect of other electrolysis technology

In use case 5; as an example of an alternative electrolysis device, input values of solid oxide electrolysis technology are used. This assessment can be useful to evaluate the impact of an electrolysis unit with performance parameters that deviate from the default values. In this example, wholesale electricity is selected as the electricity source and Norway as the country of examination. Again, Norway is chosen as it has almost a 100% green grid, allowing RFNBO hydrogen to be produced over the entire year with grid electricity.

Use case 5: Based on full year operation in Norway, does solid oxide electrolysis allow to produce hydrogen more cost-effectively compared to alkaline technology?

As depicted in Figure 12, the data related to the characteristics of the electrolysis unit are adapted and reflect the KPIs for solid oxide electrolysis expressed in the Strategic Research and Innovation Agenda 2021 – 2027 (SRIA) by the Clean Hydrogen Joint Undertaking, in addition to the Danish Energy Agency Technology Data for Renewable Fuels. This includes a CAPEX of 4000 EUR/kW, stack durability of 20,000 hours (and stack degradation of 0.6% each 1000 hours), electricity consumption of 40 kWh/kg (assuming access to nearby waste heat for free) and other OPEX amounting to 12% of CAPEX per year.

Furthermore, the electricity source data were also adapted. Specifically, adjustments were made to the operating hours and the average electricity costs. For alkaline electrolysis, the analysis relied on the 4,000 cheapest hours, whereas for solid oxide electrolysis, it is assumed that the unit operates on a 24-hour basis throughout the entire year with a minimal delay due to maintenance (8,500 hours per year). This adjustment is made to accommodate for the lower dynamic response time and to avoid losing temperature during hours of no operation. The average electricity costs were therefore computed by averaging the electricity costs over the entire year, as opposed to considering only the 4000 cheapest hours, which results in an average electricity cost of 56.39 EUR/MWh for Norway in 2023.

As a result, the LCOH calculator output (Figure 13) indicates that solid oxide electrolysis, based on the parameters used, is still 2.58 EUR/kg more expensive compared to alkaline electrolysis.

All individual cost components contributing to the total LCOH changed. Despite lower CAPEX, due to higher operating hours, and lower grid fees and taxes, due to lower energy consumption, the electricity costs and other OPEX are significantly higher for solid oxide electrolysis in this example. Noteworthy is the increase in other OPEX, where solid oxide incurs a cost that is 2.77 EUR/kg higher compared to alkaline, mainly due to the lower durability and high maintenance costs. As for the electricity cost component, note that this can be further optimized by using less operating hours at a lower average electricity price.

Use Case 5

Calculation method User specified values Electrolysis technology Solid oxide electrolysis Electricity source Wholesale **Country** Norway



Figure 12. Use case 5 – User specified data input for changing the electrolysis technology compared to default values.



All LCOH components changed

Figure 13. Use case 5 - effect of changing the electrolysis technology on the LCOH output.

Use case 6 – Effect of combining multiple electricity sources

In use case 2, which evaluates the costeffectiveness of utilizing wholesale or PV as the electricity source for hydrogen production in Spain via alkaline electrolysis, it is found that while PV has a lower LCOH, the CAPEX component is still significantly higher due to limited operating hours. Therefore, this use case showcases the effect of increasing the operating hours by using grid electricity additional to PV electricity. Use case 6: Can a combination of PV and wholesale electricity result in a lower LCOH? With alkaline electrolysis in Spain?

In this use case, the electricity source data are manually configured, as shown in Figure 14. These values are derived from calculations using the default data for wholesale and PV sources, as outlined in Table 7 using the Equation 27. The equation was used for the computation of each individual cost, including average electricity cost, grid fees, and taxes. This calculation reflects the extra added grid operating hours with the assumption that the same default prices can be used for electricity cost, grid fees and taxes.

Electricity source	Wholesale	PV	Wholesale + PV		
Operating hours (h)	1197	2803	4000		
Average electricity cost (EUR/MWh)	51.11	28.66	35.38P		
Grid fees (EUR/MWh)	11.50	0	3.44		
Taxes (EUR/MWh)	4.50	0	1.35		
$Combined cost (EUR/MWh) = \frac{\left(operating hours PV(h) \times cost PV\left(\frac{EUR}{MWh}\right) + operating hours wholesale(h) \times cost wholesale(\frac{EUR}{MWh}\right)\right)}{Total magneting hours (h)}$					

Table 7. Input data for LCOH calculation with different electricity sources.

Equation 27. Calculation of the input data for the combined energy source (wholesale + PV) with default data from individual energy sources.

As a result, in Figure 15, the LCOH calculator output indicates that, for a company intending to establish an electrolysis plant utilizing alkaline technology in Spain incorporating grid electricity alongside PV energy, a lower LCOH is achieved compared to using wholesale electricity alone, or relying solely on PV. This combined approach presents a notable advantage in reducing the CAPEX component compared to relying solely on PV energy and yielding a higher hydrogen output.



General parameters	Units	Default values
Cost of capital: Economic lifetime:	% Years	6.00% 25
Electrolysis unit Installed power: CAPEX: Energy consumption: Stack durability: Stack degradation: Stack replacement costs: Other OPEX:	kW EUR/kW kWh/kg h % per 1000h % CAPEX % CAPEX	20,000 2,310 52.40 80,000 0.12% 15.00% 2.00%
Electricity source Operating hours: Average electricity costs: Grid fees: Electricity taxes:	h/year EUR/MWh EUR/MWh EUR/MWh	4,000 51.11 11.50 4.500
Subsidies and additional revenues Electrolyser CAPEX subsidy: Hydrogen feed-in tariff or green premium: Reduction of grid fees or electricity taxes: Oxygen sale price:	EUR/kW EUR/kg EUR/MWh EUR/t	0 0 0 0

	Units	Default values
General parameters Cost of capital: Economic lifetime:	% Years	6.00% 25
Electrolysis unit Installed power: CAPEX: Energy consumption: Stack durability: Stack degradation: Stack replacement costs: Other OPEX:	kW EUR/kW kWh/kg h % per 1000h % CAPEX % CAPEX	20,000 2,310 52.40 80,000 0.12% 15.00% 2.00%
Electricity source Operating hours: Average electricity costs: Grid fees: Electricity taxes:	h/year EUR/MWh EUR/MWh EUR/MWh	2,803 28.66 0 0
Subsidies and additional revenues Electrolyser CAPEX subsidy: Hydrogen feed-in tariff or green premium: Reduction of grid fees or electricity taxes: Oxygen sale price:	EUR/kW EUR/kg EUR/MWh EUR/t	0 0 0 0

€

	Units	User specified value
General parameters		
Cost of capital:	%	6.00%
Economic lifetime:	Years	25
Electrolysis unit		
Installed power:	kW	20,000
CAPEX:	EUR/kW	2.310
Energy consumption:	kWh/kg	52.40
Stack durability:	h	80.000
Stack degradation:	% per 1000h	0.12%
Stack replacement costs:	% CAPEX	15.00%
Other OPEX:	% CAPEX	2.00%
Electricity source		4.000
Operating hours:	h/year	25.29
Average electricity costs:	EUR/MWh	244
Grid fees:	EUR/MWh	125
Electricity taxes:	EOR/MWN	1.55
Subsidies and additional revenues		0
Electrolyser CAPEX subsidy:	EUR/kW	0
Hydrogen feed-in tariff or green premium:	EUR/kg	0
Reduction of grid fees or electricity taxes:	EUR/MWh	0
Oxygen sale price:	EUR/t	L



Figure 14. Use case 6 – User specified data input for a combined electricity source compared to default values.



Use case 7 - Effect of subsidies and additional revenues

Use case 7 examines the impact on the LCOH as estimated in use case 6, considering the incorporation of financial incentives provided by governmental or other entities to promote hydrogen production, along with additional revenues from the sale of oxygen generated during the hydrogen production process.

Use case 7: How does the inclusion of subsidies and the sale of oxygen impact the hydrogen production cost? What is the effect on use case 6?

As depicted in Figure 16, in this use case, it is assumed that the project illustrated in use case 6, receives a subsidy for reducing hydrogen production costs by 2 EUR/kg, a grant of 400 EUR/kW and a reduction of grid fees and electricity taxes by 5 EUR/MWh. Moreover, they are able to sell the produced oxygen at 50 EUR/ton (extra process costs included).

As a result, the LCOH calculator output (Figure 17) reveals a significant impact when integrating these subsidies and additional revenues, reducing the LCOH with a factor of over 2.

Use Case 7	ulation method pecified values	Electrolys Alkaline electr	is technology olysis	Electricity source Wholesale + PV	ce Coun Spain	try
Combine	d (Wholesale + PV)			Combined (W with subsidies and	/holesale + P\ additional re	() venues
	Units	User specified values			Units	User specified value
Seneral parameters Cost of capital: Economic lifetime: Electrolysis unit nstalled power: CAPEX: Energy consumption: Stack durability: Stack degradation: Stack replacement costs: Other OPEX:	% Years KW EUR/kW kWh/kg h % per 1000h % CAPEX % CAPEX	6.00% 25 20.000 2.310 52.40 80.000 0.12% 15.00% 2.00% 2.00%	General Cost of d Econom Installed CAPEX: Energy Stack de Stack de Stack re Other O	parameters sapital: ic lifetime: ysis unit l power: consumption: urability: egradation: placement costs: PEX:	% Years EUR/kW KWh/kg h % per 1000h % CAPEX % CAPEX	6.00% 25 20.000 2.310 52.40 80.000 0.12% 15.00% 2.00%
Electricity source Operating hours: Average electricity costs: Grid fees: Electricity taxes:	h/year EUR/MWh EUR/MWh EUR/MWh	4.000 35.38 3.44 1.35	Electric Operatir Average Grid fee Electricit	ity source g hours: e electricity costs: s: ty taxes:	h/year EUR/MWh EUR/MWh EUR/MWh	4.000 35.38 3.44 1.35
Subsidies and additional revenues Electrolyser CAPEX subsidy: Hydrogen feed-in tariff or green premium: Reduction of grid fees or electricity taxes: Dxygen sale price:	EUR/kW EUR/kg EUR/MWh EUR/t	0 0 0 0	Subsidi Electroly Hydroge Reductio Oxygen	es and additional revenues /ser CAPEX subsidy: n feed-in tariff or green premium: on of grid fees or electricity taxes: sale price:	EUR/kW EUR/kg EUR/MWh EUR/t	400 2 5 50





<u>New</u>Use case 8 - Effect of cost of capital and economic lifetime

In use case 8; the impact of adjusting the general parameters of the electrolysis unit, specifically the cost of capital and the economic lifetime, is examined. The analysis focuses on alkaline electrolysis technology in France, with wholesale electricity as the selected source.

This analysis can be useful if the cost of capital or economic lifetime parameters of a specific project deviate from the default values used in the calculator.

Use case 8: What is the impact of a higher cost of capital and lower economic lifetime compared to the default values for alkaline technology in France using wholesale electricity?

As depicted in Figure 18, the data related to the general parameters of the electrolysis unit are adapted setting the cost of capital at 8% and the economic lifetime at 15 years, compared to the default values of 6% and 25 years, respectively³.

This scenario applies when a project developer requires a higher return on the equity and debt spend on the capital needed in the project (8% instead of 6%) and wishes a return on investment over a period of 15 years instead of 25 years.

As a result, the LCOH calculator output (Figure 19) indicates that applying these user specified values leads to a higher LCOH, which is 0.98 EUR/kg more expensive than the outcome under the default parameters.

The most substantial difference is observed in the CAPEX cost component, which rises by 1.19 EUR/kg, due to the higher cost of capital and lower economic lifetime. The other OPEX reduces by 0.19 EUR/kg, which is related to the lower economic lifetime and thus no longer needing a stack replacement. Finally, the grid fees and electricity costs are also slightly reduced due to a lower average electricity consumption related to the lower economic lifetime..

³Note: When selecting the "user specified" option, users are advised to first manually change the default values corresponding to the selected parameters in the filters as a baseline, before adjusting any additional parameters.

Use Case 8

Calculation method User specified values Electrolysis technology Alkaline Electricity source Wholesale

Country France

Perform calculations using:	Ceneral parameters Cost of capital: Economic lifetime:	Units %	Default values	User specified values		
User specified Select country France Vholesale Select electrolysis technology Akaline	Economic metime: Electrolysis unit Installed power: CAPEX: Energy consumption: Stack degradation: Stack replacement costs: Other OPEX: Electricity source Operating hours: Average electricity costs: Grid fees: Electricity taxes: Subsidies and additional revenues Electrolyser CAPEX subsidy: Hydrogen feed-in tariff or green premium: Reduction of grid fees or electricity taxes: Oxygen sale price:	kW EUR/kW kWh/kg h % CAPEX % CAPEX % CAPEX h/year EUR/MWh EUR/MWh EUR/kW EUR/kW EUR/kg EUR/kW EUR/kW	20,000 2,310 52.40 80,000 0.12% 15.00% 2.00% 4,000 59.51 14.60 1.400 0 0 0 0	20.000 2.310 52.40 80.000 0.12% 10.0% 2.00% 15.00% 2.00% 14.000 14.60 14.0 0 0 0 0 0 0	\rightarrow	Default values changed All values related to the general parameters: cost of capital and economic lifetime



Appendix

A.1. Calculation of the average energy consumption over the economic lifetime of the project

This appendix presents the evolution of the energy consumption over the economic lifetime of an electrolysis unit. Identical to the default values, a 25 year economic lifetime is adopted for the analysis, operating 4000 hours annually. The initial energy consumption is set at 52.4 kWh per kg of hydrogen produced, with a stack durability of 80,000 hours and a degradation rate of 0.12% per 1000 hours.

As shown in Figure 20 the average energy consumption is gradually increasing over the

years reaching its highest point of 57.1 kWh/kg after 19 years, corresponding to 76,000 operating hours. At the 20th year, the stack reaches the end of its 80,000-hour durability and is replaced. It is assumed that this replacement resets the energy consumption back to its initial value of 52.4 kWh/kg, initiating a new cycle of gradual increase until the next stack replacement. Table 8 provides a detailed overview of the average energy consumption across the 25-year economic lifespan of the installation.



Figure 20. Energy consumption (kWh/kg) throughout the 25-year economic lifetime of an electrolysis unit operating 4000 hours annually at a degradation rate of 0.12% per 1000 hours.

Table 8. Evolution of the energy consumption (kWh/kg) throughout the 25-year economic lifetime of an electrolysis unit operating 4000 hours annually at a degradation rate of 0.12% per 1000 hours.

Operating hours	Years	Energy consumption (kWh/kg)
0	1	52.4
4,000	2	52.7
8,000	3	52.9
12,000	4	53.2
16,000	5	53.4
20,000	б	53.7
24,000	7	53.9
32,000	8	54.2
36,000	9	54.4
40,000	10	54.7
44,000	11	55.0
48,000	12	55.2
52,000	13	55.5
56,000	14	55.8
60,000	15	56.0
64,000	16	56.3
68,000	17	56.6
72,000	18	56.8
76,000	19	57.1
80,000 (stack replacement)	20	52.4
84,000	21	52.7
88,000	22	52.9
92,000	23	53.2
96,000	24	53.4
100,000	25	53.7
	Average energy consumption	54.3